Probability distributions of continuous variables. Probability density function  $\Pr[a < x < b] = \int^{b} F(x) dx.$ F(K) = Probability density function A = Pr[acx < 67 = Sabrer dr. F(x)  $P_r Z \times < x_i ] = \int_{-\infty}^{\infty} f(x) dx$ X 5 PCKI)~ (PER'dX. continuous. Pisertete (pex) dx =1 normal Listribution  $F(X) = \frac{1}{6\sqrt{2\pi}} e^{-\frac{(X-U)^2}{262}}$ 

Binomial distribution

For only two possible outcomes: head or tail, success or failure, defective item or good item.

Let the probability that an item is dependive be p. so the probability that an item is good. be  $9 \cdot 50 \text{ the probability that an item is good.}$ 

Let the pixed no. of trial be n.

Then the general expression for the probability. OF exactly r depective items. in any order in a trial

 $\Pr[r=r] = nC_r P^r q^{n-r}$ 

 NI	pr.	gni
r! (n=r)!		

Frederic A company is considering drilling. Four oil Old wells. Probability of success per each well is 0.4, indedending of the results for each well is 0.4, indedending of the results for any other well. The cost of pack owell is \$200,000. Each well that is successful will be worth \$ 600,000. Each well that is successful will be worth \$ 600,000. b) what is expected number of successful b) what is expected gain.? b) what is expected gain.? c) what is probability of a loss. b) what is probability of a loss. b) what is stantorf deviation?

 $\frac{Varience}{\Sigma} (x_i - u)^2 / N$  $6_{x}^{2} = E(x - u_{x})^{2} = mean(x - u_{x})^{2}$  $= \sum (X - U_{R})^{2} Pr(X_{i}).$  $6x^2 = \Xi [x^2] - ux^2$  $= E [x^2 - 2M_x X + M_x^2]$  $= E[x^2] - 2u_x E[x] + u_x$  $= E [x^2] - 2u^2 + u^2$  $= E [x^2] - M_x$  $E[x^2] = 5 x_i^2 P_r(x_i).$ standard deviation N6x = 6x.  $E(R^{2}) = 0^{2} \times \frac{1}{32} + (1)^{2} + 2^{2} \frac{10}{32} + 3^{2} \frac{10}{32} + 4^{2} \frac{1}{32} + 5^{2} \frac{10}{32} + 5^{2} \frac$ = 7.5.  $-\frac{1}{6x} = 7.5 - (4R)^{2} = 7.5 - (2.5)^{2} = 1.2.5$ Sta. 6x = V1.25 = 1-118

Poisson Distribution (s. D. Poisson, French Mathematic

4 counts from Geiger Counter.

collisions of ravy at specific intersoction under specific condition,

Flows in rowling Probability of r occurrences in a fixed interval of time or space under particular condition. is given by.

 $\Pr\left[R=r\right] = \frac{(\lambda t)^{r}e^{-\lambda t}}{r!}$ t = interval of time or space in which events occur. A = mean rate of occurrence per unit time or space. Xt = dimensionless

Pr[R=rH] = (M+) Pr[R=r]I the number of meteors found by a radar system in any 30-seeinterval under specified conditions averages 1-81. Assume it appear randomly and independently.

of what is the probability that no meteors are found in a one-minute interval?

67 Find Pr [8 >>r 5>5].  $\lambda = 1.81/0.5$  for mint = 3.62 mint.  $: t = 1; 4 = \lambda t = 3.62 \times 1 = 3.62$ .  $\Pr[r=0] = e^{-3.62} = 0.0268$ 

b) 11 = > += 3.62 ×2 = 7.24 occurance in 2 minute.  $PrTR=5] = (7.24)^5 e^{-7.24}$ 51 = 0.1189 Pr[R=0] = At pr[R=0]  $\Pr[R=6] = \frac{7\cdot 24}{6} \quad 0 \cdot 1189 = 0 \cdot 1435$  $\Pr[R=7] = \frac{7.24}{7} \times 0.1435 = 0.1484$  $\Pr[R=8] = \frac{7\cdot24}{8} \times 0.1484 = 0.1343$  $fr[5 \le r \le 8] = 0.1189 \pm 0.1435 \pm 0.1484 \\ \pm 0.1343$ Consignation property in = 0.545CLIMBER DURING

## Probability Distributions of Discrete Variables



Then 
$$\bar{x} = \frac{\sum f_i x_i}{\sum f_i} = \frac{115}{40} = 2.875$$
. Then take  $\mu = \lambda t = 2.875$  in 6 minute  
Then  $\lambda = \frac{\lambda t}{t} = \frac{2.875}{6} = 0.479$  cars / minute.

According to the Poisson Distribution, then,  $\Pr[R=r] = (2.875)^r e^{-2.875}/ r!$ . It was mentioned previously that once one of the Poisson probabilities is calculated, others can be calculated conveniently using the recurrence relation of equation 5.14,

$$\Pr\left[R=r+1\right] = \left(\frac{\lambda t}{r+1}\right)\Pr\left[R=r\right].$$

Calculation of Poisson probabilities and relative frequencies gives the following results:

r	$f_i$	<b>Pr</b> [ <i>R</i> = <i>r</i> ]	Relative Frequency	OFE(X)
0	2	0.0564	0.0500	447
1	7	0.1622	0.1750	$= \frac{4 + 7}{4 + 1}$
2	10	0.2332	0.2500	40
3	8	0.2234	0.2000	= 11075
4	6	0.1606	0.1500	2
5	3	0.0923	0.0750	6 = 11-175 - MK
6	3	0.0442	0.0750	ox
7	1	0.0182	0.0250 4.9	= 2 - 9093
>8	0	0.0095	0	0 -1 -70 -1
Total	40	1999-1999-1995-1995- 1995-1996-1996-1995-1995-1995-1995-1995-	Sum = 447	6x = 107056

The frequencies from the problem statement are compared with the calculated expected frequencies in Figure 5.18. It can be seen that the agreement between

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FCX) gaudion

Probability & It is a measure of the likelihood that a particular event occur. probability distribution of discrete variable Probability function Liscrete random Variable X are Xo XI X2 ..... XK P(xo) P(xi) P(xz) . - P(XK) . Probabilities p(xi)>0 and Ep(xi)=1. P(x;) = Probability punction P(x)04 . 027 · 017 · 0 0 1 2x 3 4 5 6 7 8 cumulative distribution Function  $\Pr[X \leq x] = \sum p(x_i).$  $Pr[X \leq 3] = P(X_0) + P(X_1) + P(X_2) + P(X_3)$ = p(0) + p(1) + p(2) + p(3)Pr[X K2] = P(0) + P(1) + P(2) (3) = Pr[X53] - Pr[X52]. p(xi) = pr[x<xi] - pr[x<xi]

 $f > 6x^2 = E(x^2) - 4x^2$  $E(x)^2 = 3.5200 \cdot 4x = 1.6$  $-6x^{2} = 3.5 - (1.6)^{2} = 0.96$  $6x = \sqrt{0.96} = 0.98$ Reference ! W.J. De Coursey, Statistics and Probability for Engineering Applications.

A distillation process is shown in Figure. You are asked to solve for all of the values
of the stream flows and compositions. Explain each answer and show all details of
how you reached your decision. For each stream (except *F*), the only components
that occur are labeled below the stream. Solve the system by *Matlab* function.



Figure shows a simplified process to make ethylene dichloride (C<sub>2</sub>H<sub>4</sub>Cl<sub>2</sub>). The feed data have been placed on the figure. Ninety percent conversion of the C<sub>2</sub>H<sub>4</sub> occurs on each pass through the reactor. The overhead stream from the separator contains 98% of the Cl<sub>2</sub> entering the separator, 92% of the entering C<sub>2</sub>H<sub>4</sub>, and 0.1% of the entering C<sub>2</sub>H<sub>4</sub>Cl<sub>2</sub>. Five percent of the overhead from the separator is purged. Calculate (a) the flow rate and (b) the composition of the purge stream using *Matlab* function.



 Two interacting tank in series with outlet flow rate being function of the square root of tank height. Write mass balance (ordinary differential equation) equations of two tanks assuming no change of density in the system.



F=5 ft<sup>3</sup>/min, A<sub>1</sub>=5 ft<sup>2</sup>, A<sub>2</sub>=10 ft<sup>2</sup>, R<sub>1</sub>=2.5 ft<sup>2.5</sup>/min,

Solve two equations with ode45 function in Matlab and find  $h_2$  in the time range from t=0 min to t=150 min. At t=0,  $h_1(0)=12$  and  $h_2(0)=7$ .

• Consider the stirred Tank Heater System (Figure): Total momentum of the system remains constant and will not be considered. Write total mass balance: Total mass in the tank at any time t =rV = rAh where A represents cross sectional area, h represents height of liquid and r represents density of the liquid. Assuming that the density is independent of the temperature and remains constant. Take  $F = 0.02236\sqrt{h}$ . Write energy balance equation considering no change in kinetic energy and potential energy. For liquid system assume change of internal energy same as enthalpy change. Heat given through steam is Q=10 kW and it is remains unchanged. Solve total mass balance and energy balance equations with state variables h (in material balance) and T (in energy balance) by **Matlab** ode solver with initial gauss of T=30°C and h=0.1 m. Find the steady state h and steady state T of the tank. Take inlet temperature of the tank T<sub>i</sub>=30°C, inlet flow rate of the tank F<sub>i</sub>=0.01 m<sup>3</sup>/min. A=1 m<sup>2</sup>, r=1000 kg/m<sup>3</sup>, C<sub>p</sub>=2000 J/kg.



## • Vapor-Liquid equilibrium for ideal mixture

A liquid mixture contains 50% pentane (1), 30% hexane (2) and 20% cyclohexane (3) (all in mol-%), i.e., X1 = 0.5; X2 = 0.3; X3 = 0.2. At T = 400 K, the pressure is gradually decreased. Estimate bubble pressure and composition of the first vapor that is formed using *Matlab-generated code*. Assume ideal liquid mixture and Ideal gas (Raoult's law).

Components	Α	В	С
pentane	3.97786	1064.840	-41.136
hexane	4.00139	1170.875	-48.833
cyclohexane	3.93002	1182.774	-52.532

Where, 
$$log_{10}P_{sat}(bar) = A - \frac{B}{T(K)+C}$$

Consider the liquid mixture with 50% pentane (1), 30% hexane (2) and 20% cyclohexane (3) (all in mol-%). At p = 5 bar, the temperature is gradually increased. Estimate bubble temperature and composition of the first vapor that is formed using *Matlab-generated code*. Assume ideal liquid mixture and Ideal gas (Raoult's law).

- A vapor mixture contains 50% pentane (1), 30% hexane (2) and 20% cyclohexane (3) (all in mol-%), i.e., Y1 = 0.5; Y2 = 0.3; Y3 = 0.2. At T = 400 K, the pressure is gradually increased. Estimate dew-point pressure and composition of the first liquid that is formed using *Matlab-generated code*. Assume ideal liquid mixture and Ideal gas (Raoult's law).
- 4. A vapor mixture contains 50% pentane (1), 30% hexane (2) and 20% cyclohexane (3) (all in mol-%), i.e., Y1 = 0.5; Y2 = 0.3; Y3 = 0.2. At P = 5 bar, the temperature is gradually decreased. Estimate dew-point T and composition of the first liquid that is formed using *Matlab-generated code*. Assume ideal liquid mixture and Ideal gas (Raoult's law).

## • Vapor-Liquid equilibrium for non ideal mixture

1. Estimate the bubble point temperature and vapor composition for a acetone (1) and water (2) liquid mixture with  $x_1 = 0.01$  at a total pressure of 101.3 kPa6 with a *Matlab* code. Use the Wilson model with the parameters:

Components	Λ <sub>12</sub>	Λ <sub>21</sub>
Acetone	0.1173	0.4227
Water		

$$lnP_{sat}^{1}(kPa) = 14.71712 - \frac{2975.95}{T(K) - 34.5228}$$
$$lnP_{sat}^{2}(kPa) = 16.5362 - \frac{3985.44}{T(K) - 38.9974}$$

2. Construct a Txy diagram for a mixture of ethanol (1) with hexane (2) at a total pressure of 101.3 kPa with a *Matlab* code. Use the Wilson model with the parameters  $\Lambda_{12} = 0.0952$ ,  $\Lambda_{21} = 0.2713$ . Vapor pressure: ( $P_{sat}^i$  in kPa and T in °K)

$$lnP_{sat}^{1}(kPa) = 16.1952 - \frac{3423.53}{T(K) - 55.7172}$$
$$lnP_{sat}^{2}(kPa) = 14.0568 - \frac{2825.42}{T(K) - 42.7089}$$

Wilson

$$\ln \gamma_{1} = -\ln[x_{1} + x_{2}\Lambda_{12}] + x_{2}\left[\frac{\Lambda_{12}}{x_{1} + x_{2}\Lambda_{12}} - \frac{\Lambda_{21}}{x_{2} + x_{1}\Lambda_{21}}\right]$$
$$\ln \gamma_{2} = -\ln[x_{2} + x_{1}\Lambda_{21}] + x_{1}\left[\frac{\Lambda_{21}}{x_{2} + x_{1}\Lambda_{21}} - \frac{\Lambda_{12}}{x_{1} + x_{2}\Lambda_{12}}\right]$$

Aromatics, alcohol, ketones, ethers, C<sub>4</sub>-C<sub>18</sub> hydrocarbons